

## Erratum

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CFD simulation of bubble column flows: Investigations on turbulence models in RANS approach

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**The color code of the figures captions follow:**

#### FIGURE CAPTIONS

Fig. 1. Radial profiles of the liquid axial velocity in the case of the Dispersed Standard  $k$ - $\varepsilon$  model for grid #1, using 1<sup>st</sup> order Upwind (♦), 2<sup>nd</sup> order Upwind (◆) and 3<sup>rd</sup> order MUSCL schemes (◇). Comparison with CARPT data (♦) given by Chen (2004).

Fig. 2. Radial profiles of the gas holdup in the case of the Dispersed Standard  $k$ - $\varepsilon$  model for grid #1, using 1<sup>st</sup> order Upwind (♦), 2<sup>nd</sup> order Upwind (◆) and 3<sup>rd</sup> order MUSCL schemes (◇). Comparison with CT data (♦) given by Chen (2004).

Fig. 3. Radial profiles of the liquid axial velocity in the case of the Dispersed RNG  $k$ - $\varepsilon$  model for grid #1 (♦), grid #2 (◆), grid #3 (◇), grid #4 (◇), grid #5 (◆), grid #6 (◆) and grid #7 (◆).

Fig. 4. Radial profiles of the gas holdup in the case of the Dispersed RNG  $k$ - $\varepsilon$  model for grid #1 (♦), grid #2 (◆), grid #3 (◇), grid #4 (◇), grid #5 (◆), grid #6 (◆) and grid #7 (◆).

Fig. 5: Radial profiles of the liquid axial velocity in the case of the Standard  $k$ - $\varepsilon$  model for the Dispersed ( $\blacklozenge$ ), Dispersed + BIT ( $\blacklozenge$ ), and Per-phase ( $\blacklozenge$ ) options. Comparison with CARPT data ( $\blacklozenge$ ) given by Chen (2004).

Fig. 6. Radial profiles of the gas holdup in the case of the Standard  $k$ - $\varepsilon$  model for the Dispersed ( $\blacklozenge$ ), Dispersed + BIT ( $\blacklozenge$ ), and Per-phase ( $\blacklozenge$ ) options. Comparison with CT data ( $\blacklozenge$ ) given by Chen (2004).

Fig. 7. Radial profiles of the liquid axial velocity in the case of the Realizable  $k$ - $\varepsilon$  model for the Dispersed ( $\blacklozenge$ ), Dispersed + BIT ( $\blacklozenge$ ), and Per-phase ( $\blacklozenge$ ) options. Comparison with CARPT data ( $\blacklozenge$ ) given by Chen (2004).

Fig. 8. Radial profiles of the gas holdup in the case of the Realizable  $k$ - $\varepsilon$  model for the Dispersed ( $\blacklozenge$ ), Dispersed + BIT ( $\blacklozenge$ ), and Per-phase ( $\blacklozenge$ ) options. Comparison with CT data ( $\blacklozenge$ ) given by Chen (2004).

Fig. 9. Radial profiles of the liquid axial velocity in the case of the RNG  $k$ - $\varepsilon$  model for the Dispersed ( $\blacklozenge$ ), Dispersed + BIT ( $\blacklozenge$ ), and Per-phase ( $\blacklozenge$ ) options. Comparison with CARPT data ( $\blacklozenge$ ) given by Chen (2004).

Fig. 10. Radial profiles of the gas holdup in the case of the RNG  $k$ - $\varepsilon$  model for the Dispersed ( $\blacklozenge$ ), Dispersed + BIT ( $\blacklozenge$ ), and Per-phase ( $\blacklozenge$ ) options. Comparison with CT data ( $\blacklozenge$ ) given by Chen (2004).

Fig. 11. Radial profiles of instantaneous, circum- and axially-averaged turbulent kinetic energy for the Standard  $k$ - $\varepsilon$  model Dispersed ( $\blacklozenge$ ), Standard  $k$ - $\varepsilon$  model Per-phase ( $\blacklozenge$ ), Realizable  $k$ - $\varepsilon$  model Dispersed ( $\blacklozenge$ ), Realizable  $k$ - $\varepsilon$  model Per-phase ( $\blacklozenge$ ), RNG  $k$ - $\varepsilon$  model Dispersed ( $\blacklozenge$ ), RNG  $k$ - $\varepsilon$  model Per-phase ( $\blacklozenge$ ).

Fig. 12. Radial profiles of instantaneous, circum- and axially-averaged turbulent dissipation rate for the Standard  $k$ - $\varepsilon$  model Dispersed ( $\blacklozenge$ ), Standard  $k$ - $\varepsilon$  model Per-phase

(♦), Realizable  $k$ - $\varepsilon$  model Dispersed (♦), Realizable  $k$ - $\varepsilon$  model Per-phase (♦), RNG  $k$ - $\varepsilon$  model Dispersed (♦), RNG  $k$ - $\varepsilon$  model Per-phase (♦).